

Significant room temperature oxygen storage over 0.58% Pt/Ce_{0.68}Zr_{0.32}O₂ when H₂ is used as a reducing agent

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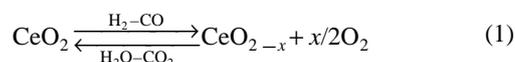
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The investigation of the oxygen storage/release capacity (OSC) of 0.58 wt% Pt/Ce_{0.68}Zr_{0.32}O₂ catalyst by oscillating the feed-stream between reducing and oxidising conditions showed that a high OSC could be measured at room temperature, even for redox-aged sample, by using H₂ as the reducing agent.

The so-called oxygen storage/release capacity (OSC) of a three-way catalyst (TWC) is the ability to attenuate the negative effects of rich/lean oscillations of exhaust gas composition. By maintaining a stoichiometric composition at the catalyst, the highest conversion efficiency of the exhaust is attained. OSC, which in the modern TWCs is achieved by adding a CeO₂-ZrO₂ mixed oxide component, is usually discussed in terms of the ability to regulate the oxygen partial pressure in the exhaust through the Ce³⁺/Ce⁴⁺ redox couple [eqn. (1)]:



Formation of vacancies is therefore either implied or assumed. Following the pioneering work of Yao and Yu-Yao,¹ dynamic-OSC measurement involves alternately pulsing the chosen reducing agent (usually CO but sometimes H₂) and O₂ over the material under investigation. More recently the oxygen buffering capacity (OBC) technique has been developed by Bernal *et. al.*² In this method O₂ is pulsed over the sample in a flow of inert gas, which effectively corresponds to oscillations between mildly reducing and oxidising conditions.

Here, we demonstrate that it is possible, using H₂ as reducing agent, to measure significant dynamic-OSC over Pt/Ce_{0.68}Zr_{0.32}O₂ under conditions where vacancy creation is unlikely (room temperature, r.t.). Such high r.t. OSC is not observed when either CO is used as reductant or when the OBC method is employed. The evidence suggests that this dynamic-OSC may be associated with the phenomenon of spillover. This opens the possibility that spilled-over H₂ can be a contributing factor to OSC measurements even at higher temperatures. The presence of H₂ in exhaust effluent in a ratio of *ca.* 1:3 with respect to CO³ makes this finding a potentially important piece of information.

0.58 wt% Pt/Ce_{0.68}Zr_{0.32}O₂ and 0.53 wt% Pt/CeO₂ were prepared and supplied by RHODIA as part of the CEZIR-ENCAT network.⁴ 0.5 wt% Pt/γ-Al₂O₃ (γ-Al₂O₃: Alfa products) was prepared using Pt(NH₃)₂(NO₂)₂ as precursor. An *in situ* oxidising cleaning procedure⁵ (heating in flow of O₂ at 823 K for 1 h) was applied before all experiments, giving a sample designated as fresh. Redox-aged sample was prepared as follows: reduction up to 1273 K in 5% H₂ in Ar (25 ml min⁻¹), holding at 1273 for 15 min, flushing in Ar at 1273 K; slow cooling to 700 K; re-oxidation at 700 K and cooling to 423 K in 5% O₂ in Ar; and, finally, cooling to r.t. in Ar (60 ml min⁻¹). Quantitative dynamic-OSC measurements were performed by increasing the temperature in a stepwise manner and, during the isothermal steps (60 min), alternately pulsing every 70 s H₂ (500 or 100 μl, H₂-OSC) or CO (100 μl, CO-OSC) and O₂ (250 or 100 μl) over the sample (20 mg, maintained in a flow of Ar of

25 ml min⁻¹). OSC was measured using a thermal conductivity detector as the uptake of O₂ from the O₂ pulse. Steady-state values are reported. When CO was used as the reducing agent, the evolved CO and CO₂ were separated on a Porapak Q column. TPR-MS profiles were obtained up to 1273 K as above reported for redox-ageing. OBC measurements were carried out as reported previously.² Hydrogen chemisorption measurements were conducted at 298 and 195 K.⁶

The redox behaviour was first investigated by means of the TPR-MS technique. The TPR profiles (not reported) of fresh and redox-aged Pt/Ce_{0.68}Zr_{0.32}O₂ showed single reduction features centred around 500 and 400 K, respectively. This behaviour is fairly consistent with a recent report⁶ and is attributed to an initial reduction of supported PtO, which in turn results in support reduction through spillover of hydrogen species. The degree of reduction, *i.e.* the overall transferable oxygen, was measured by O₂ uptake at 700 K after the TPR experiment as previously reported.⁶ An O₂ uptake of 20 ml g⁻¹ was obtained for both fresh and redox-aged samples.

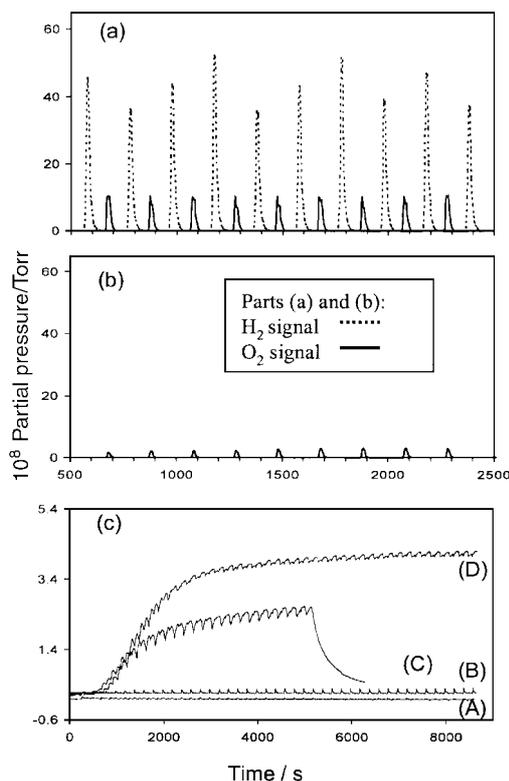


Fig. 1 H₂-OSC measured at r.t. H₂ (*m/z* = 2) and O₂ (*m/e* = 32) profiles over fresh/reduced at 500 K Pt/Al₂O₃ (for clarity this trace is displaced) (a) and Pt/Ce_{0.68}Zr_{0.32}O₂ (b), and water production (*m/e* = 18) (c) over: (A) fresh/reduced 500 K Pt/Al₂O₃, (B) fresh Pt/Ce_{0.68}Zr_{0.32}O₂; (C) redox-aged Pt/Ce_{0.68}Zr_{0.32}O₂, reaction stopped at 5000 s; (D) fresh/reduced 500 K Pt/Ce_{0.68}Zr_{0.32}O₂. MS was tuned to enhance the sensitivity to H₂ compared to O₂. 200 mg of sample and loop volumes of 1 ml were employed.

Table 1 Oxygen storage and chemical/textural characterisation of the Pt/Ce_{0.68}Zr_{0.32}O₂ catalyst

Sample	Oxygen storage capacity ^a /OBC ^b				H ₂ chemisorption ^c			N ₂ physisorption Surface area/ m ² g ⁻¹
	T/K	H ₂ -OSC ^d / ml O ₂ g ⁻¹	CO-OSC/ ml O ₂ g ⁻¹	OBC (%)	H ₂ uptake/ml g ⁻¹			
					T/K	0 Torr	20 Torr	
Pt/Ce _{0.68} Zr _{0.32} O ₂ fresh/reduced	r.t.	6.3	0.0		298	6.78	7.09	100
	373	7.1	0.7		193	0.31	0.37	
	473	7.5	1.7					
	673	8.1	>2.6	4				
	773	8.9	>2.6	20				
Pt/Ce _{0.68} Zr _{0.32} O ₂ redox-aged	r.t.	2.8	0.0		298	2.62	2.76	30
	373	4.1	0.0		193	0.09	0.09	
	473	9.1	0.1					
	673	9.8	>2.6	8				
	773	11.6	>2.6	21				
Pt/CeO ₂ fresh/reduced	r.t.	4.2			298	3.88	4.02	88
					193	0.30	0.31	
Pt/CeO ₂ redox-aged	r.t.	0.6			298	0.47	0.45	7
					193	0.04	0.04	
					298	0.28	0.30	
Pt/Al ₂ O ₃ fresh/reduced	r.t.	0.3			298	0.28	0.30	99
					193	0.26	0.27	

^a Quantitative analysis using TCD, standard deviation ± 0.4 ml O₂ g⁻¹. Steady state values measured as O₂ uptake (ml g⁻¹). For CO / O₂ experiments, an OSC of 2.6 ml O₂ g⁻¹ corresponds to a maximum O₂ uptake using the experimental setup described in the text. ^b OBC (%): $[100 (A_{NA} - A_A)/A_{NA}]$; A_{NA}: area under non-attenuated pulse; A_A: area under the attenuated pulse. Pulse volume 0.25 ml of 5% O₂ in He. ^c Sample reduced at 500 K for 1 h, followed by evacuation at 673 K for 4 h. A range of H₂ pressure of 2–20 Torr was employed. Adsorbed volumes were determined by extrapolation to zero pressure of the linear part of the adsorption isotherm (0 Torr). Cumulative H₂ adsorption at $p = 20$ torr is also given. ^d Using loop volumes of 100 μ l for H₂ and O₂ a full O₂ uptake, i.e. 2.6 ml O₂ g⁻¹, was observed in all experiments.

Fig. 1 compares the H₂-OSC behaviour at r.t. of Pt/Ce_{0.68}Zr_{0.32}O₂ and Pt/Al₂O₃. Table 1 summarises quantitative OSC measurements and also some characterisation data. Fresh/reduced Pt/Al₂O₃ does not exhibit appreciable H₂-OSC at r.t. In contrast, a very high consumption of both H₂ and O₂ is observed over fresh/reduced Pt/Ce_{0.68}Zr_{0.32}O₂, indicating the crucial role of the Ce_{0.68}Zr_{0.32}O₂ in providing sites for the storage process. Water evolution is also observed in the latter case [Fig. 1(c), trace D], ruling out any kind of chromatographic effect. Negligible water production is observed over the fresh Pt/Ce_{0.68}Zr_{0.32}O₂, [Fig. 1(c), trace B], indicating that reduced Pt is necessary to promote hydrogen activation. In an attempt to establish the origin of this high r.t. H₂-OSC, H₂ chemisorption measurements were carried out on the Pt/Ce_{0.68}Zr_{0.32}O₂ at 193 and 298 K. Spilling of H₂ at 193 K is negligible allowing determination of H/Pt ratios.⁷ 0.31 ml H₂ g⁻¹ are adsorbed at 193 K which correspond to a dispersion of 94% upon assumption of H:Pt = 1:1 stoichiometry. The low H₂ uptake indicates that titration of hydrogen/oxygen adsorbed on the metal cannot be responsible for the observed H₂-OSC. Conversely, the amount of H₂ adsorbed/spilled over the support at 298 K is of the same order of magnitude of the values of H₂-OSC, suggesting a relevant role of the spillover phenomena in the oxygen storage. A higher relative pressure of H₂ during the H₂ pulse and presence of H₂O could account for the high values of O₂ uptake compared to the spilt H₂ detected in the chemisorption measurement. In fact, H₂ and O₂ consumption close to stoichiometry is measured in the H₂-OSC experiment. Redox-ageing decreases both the surface area and the amount of adsorbed H₂ at 298 K by a factor of three. The H₂-OSC decreases by a factor of two. The important role of hydrogen spillover in giving high H₂-OSC at r.t. is supported by the data reported for Pt/Al₂O₃ and Pt/CeO₂. In particular, very small r.t. H₂-OSC is observed for the latter catalyst after redox-ageing, when spillover is negligible.

The comparison with CO as reducing agent and the OBC measurements is striking. Irrespective of the pre-treatment, fresh/reduced or recycled, significant CO-OSC is observed only at and above 473 K, while OBC starts being significant at 673 K. In both these experiments, the reduction process may be envisaged as a measure of the oxygen diffusion towards the

surface where it is removed either by interaction with CO or simple desorption, provided that surface processes are not rate limiting.⁸ The very high H₂-OSC clearly points to a crucial role of H₂ in affecting the redox properties of these systems at low temperatures.

In conclusion, there is a dramatic dependence of the results obtained on the nature of the reducing environment with significantly high dynamic-OSC particularly apparent at low temperatures using H₂. At r.t. spillover phenomena seem to be a dominant factor. The implications of these findings need to be carefully considered when the results of such measurements are extended to the extremely complicated conditions encountered in three-way catalysis.

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